



Enhancing Micro-Droplet Mixing in Microfluidic Systems Via Electrowetting-Induced Parametric Oscillations

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In the context of space exploration, electrowetting-on-dielectric (EWOD) microfluidic systems hold substantial promise for enhancing *in-situ* analysis and experimentation, particularly given its potential for precise control of fluid dynamics in the microgravity environment. This study investigates the effects of electrowetting-induced parametric oscillations on mixing efficiency within coalesced micro-droplets in EWOD microfluidic devices using numerical simulations. The mechanism by which parametric oscillation affects the mixing process of micro-droplets in EWOD devices is unraveled, which is previously uninverstigated in the literature to the best of our knowledge. The simulations reveal that parametric oscillations significantly increase vorticity magnitude and shear rate around the droplet interface, leading to improved mixing compared to free oscillation. Notably, the study identifies fluctuations in the mixing index associated with the oscillation-induced shape changes of the droplets. These findings underscore the potential of parametric oscillation as a strategy for optimizing mixing in EWOD systems, with implications for the design of more efficient microfluidic devices.

Keywords: electrowetting-on-dielectric (EWOD), microfluidic systems, parametric oscillation, mixing efficiency, numerical simulation

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INTRODUCTION

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Wei Y, Zou J, Zhao Z and Sun J (2025) Enhancing Micro-Droplet Mixing in Microfluidic Systems Via Electrowetting-Induced Parametric Oscillations. Aerosp. Res. Commun. 2:14205. doi: 10.3389/arc.2024.14205 Microfluidic technology plays a pivotal role in space research, particularly with the use of lab-on-chip platforms for conducting astrobiological studies in the unique conditions of microgravity and radiation exposure [1], in addition to the diagnostic tools utilized for monitoring the health and living conditions of astronauts [2, 3]. Microfluidic platforms have demonstrated their potential in facilitating complex biological experiments performed in of the International Space Station (ISS) and CubeSat missions [4, 5], offering a compact and efficient means of conducting biomedical research in microgravity. The integration of microfluidic technology in proposed NASA and ESA missions, such

as the "tissue chips" initiative [6–8] and the ESA-SPHEROIDS project [9, 10], exemplifies the progressive role of microfluidics in space biology, signaling a trend towards more advanced and integrated space research capabilities.

Electrowetting-on-dielectric (EWOD) constitutes an advanced technique in of digital microfluidics, enabling the precise manipulation of droplets with volumes ranging from picoliters to microliters [11] by modulating their wettability through the application of variable voltages, thereby facilitating the execution of complex laboratory procedures [12]. In year 2018,

EWOD-based microfluidics has been used as electrowetting heat pipes on the ISS, and key microfluidic operations (droplet motion and splitting) are examined [13]. The findings indicate that electrowetting experiments are feasible in a space environment, suggesting that concerns pertaining to safety, reliability, and compactness can be effectively addressed [14].

On the other hand, due to the small size of micro-droplets and the limited diffusivity of most analytes and reagents within biochemical analysis systems, the majority of microfluidic species transport systems operate at low Reynolds numbers (characterizing laminar flow) and high Peclet numbers (indicating minimal diffusion) [15]. This combination renders mixing within micro-droplets a significant challenge and a critical issue in the field of microfluidics. Traditional methods for enhancing droplet mixing involve moving the coalesced droplet back and forth on a grid of electrodes, which oscillates the droplet to increase the interfacial area and promote diffusive processes [16-18]. Recently, a common approach to improve micro-droplet mixing in digital microfluidics is to generate oscillations within the combined droplet by applying AC voltage [19, 20]. Resonant droplet oscillation can be triggered by applying AC voltage in the EWOD microfluidics, which has been experimentally [19, 21-26] and numerically [27] proven as an effective approach to microfluid mixing. The shape oscillation brought about by the resonance mode can induces transient and chaotic convective vortices around the droplet, which greatly accelerates the mixing process [25, 28].

There are numerous studies on the oscillation of AC voltageactuated droplets, but only a few testified to the oscillation's applicability for mixing enhancement, and most of them are experiments [27]. Therefore, more numerical simulations are required to give detailed characteristics of the fluid flow by visualization of the internal flow within the droplet [29]. Based on the above analysis, this study presents a numerical examination of the influence of parametric oscillation on the mixing process of micro-droplets within digital microfluidic systems. The parametric oscillation is induced by the application of voltages with high amplitude and a driving frequency, f_d , which is roughly double the resonance frequency of the droplet, f_n . Throughout the parametric oscillation, the mixing index, MI, displays an oscillatory pattern over time. The mixing index fluctuation, denoted as MIosc, is extracted and analyzed. Additionally, the fluid dynamics triggered by the parametric oscillation and its effects on mixing efficacy are scrutinized. Our findings elucidate the underlying mechanisms by which parametric oscillation enhances mixing in electrowetting-driven merged micro-droplets.

METHODS

In this section, the electrowetting mechanism that drives the droplet motion in digital microfluidics is introduced. A droplet manipulation scheme where the droplets are merged, oscillated, and mixed is presented. Finally, numerical models and formulations are established.



Droplet Manipulation Schemes

The manipulation of droplets in our study is based on the EWOD principle, as illustrated in **Figure 1**. The system comprises a dielectric layer, patterned electrodes, and a hydrophobic surface. A droplet, initially at rest with a contact angle θ_0 , is placed on this surface, bridging two electrodes. The application of a voltage V_{ap} to an electrode induces electrowetting, reducing the contact angle to θ_v as described by the Young-Lippmann equation (**Equation 1**).

$$\gamma \cos \theta_{\nu} - \gamma \cos \theta_0 = \frac{1}{2} C V_{ap}^2 \tag{1}$$

Where γ represents the liquid-gas surface tension coefficient, *C* denotes the dielectric layer's capacitance per unit area. A pressure gradient induced by $\theta_v < \theta_0$ propels the droplet towards the right. EWOD effect enables droplet transport by altering the contact angle, with the driving frequency f_d corresponding to half the frequency of the applied AC voltage, f_{ac} . Basic operations include transport, coalescence, division, and dispensing, typically managed through a two-dimensional electrode array [30]. **Figure 2** outlines the electrode actuation scheme for droplet merging. Initially, droplets 1 and 2, with and without dye, respectively, are positioned at the interface of electrodes 1-2 and 3-4 [**Figure 2A**]. Activation of electrodes 2 and 3 at t = 0 s induces electrowetting effect, causing the droplets to merge into droplet 3 [**Figures 2B, C**].

Before applying AC voltage to the droplet, some prepatory work are done. At $t = t_{merge1}$, all the electrodes are activated to smear out the influence of electrode 1 and 4 on the merged droplet's motion, as shown in **Figure 2D**. The droplet oscillates under a uniform electric field due to inertia. At $t = t_{merge2}$, the droplet has been fully merged and the natural oscillation amplitude has been dissipated a lot. At this time, apply AC voltage to all the electrodes. As a result, the contact angle θ constantly changes according to **Equation 1**, and the droplet mixes with oscillation. Scaled by the capillary timescale $t_c = \sqrt{\rho R_0^3 \gamma}$, the two nondimensionalized critical time \bar{t}_{merge1} and \bar{t}_{merge2} are set as 2.05 and 24.81, respectively.



droplet 3 oscillates freely.

For the simulation, the electrowetting effect is modeled by periodically varying the contact angle according to **Equation 2**, where θ_{max} and θ_{min} represent the maximum and minimum contact angles, respectively.

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$$\theta = \frac{\theta_{\max} - \theta_{\min}}{2} \sin\left(2\pi f_d t - \frac{\pi}{2}\right) + \frac{\theta_{\max} + \theta_{\min}}{2}, \quad (2)$$

This approach simplifies the numerical simulation by replacing the complex electrowetting dynamics with a sinusoidal variation of the contact angle [27, 31].

Numerical Modeling and Interface Tracking

The numerical modeling of the incompressible microfluidic flow in this study is based on the Navier-Stokes (NS) equations, which are given by **Equation 3** for the momentum conservation and **Equation 4** for the incompressibility condition.

$$\rho \frac{d\vec{u}}{dt} + \rho (\vec{u} \cdot \nabla) \vec{u} = -\nabla p + \nabla \cdot \left[\mu \left(\nabla \vec{u} + (\nabla \vec{u})^T \right) \right] + \vec{F}_{st} + \rho \vec{g} \quad (3)$$
$$\nabla \vec{u} = 0 \quad (4)$$

Where ρ is the density, \vec{u} is the velocity, p is the pressure, \vec{F}_{st} is the surface tension, \vec{g} is the gravitational acceleration, and t is time. The water droplet dimensions are on millimeter scale, resulting in a Bond number, $Bo = \frac{\rho g l^2}{\gamma}$, less than unity, where l is the droplet's characteristic length scale. Thus, gravitational forces in **Equation 3** are neglected [32].

The phase-field method is employed to track the dynamic interface of the droplet. The phase-field variable ϕ and its chemical potential *G* are introduced to replace the surface tension term \vec{F}_{st} in **Equation 3** with $G\nabla\phi$, as shown in **Equation 5**. The Cahn-Hilliard equation governs the evolution of ϕ and ensures that it assumes values of -1 or 1, except in a thin region at the fluid-fluid interface, as shown in **Equation 6**, where χ is the diffusion parameter, called the mobility:

$$\vec{F}_{st} = G\nabla\phi \tag{5}$$

$$\frac{\partial \phi}{\partial t} + \vec{u} \cdot \nabla \phi = \nabla \cdot \chi \nabla G \tag{6}$$





The mass equation, given by **Equation 7**, is used to calculate the dye concentration within the droplets, where *c* is the concentration of the solute, D_{ab} is the diffusivity, and *R* is the reaction rate. The equation describes the transport of solute within the merged droplet, where the initial concentration in one droplet is c_0 and in the other is 0. The solute spreads until the concentration is uniform throughout the merged droplet. The reaction rate *R* is set to 0 in this study.

$$\frac{\partial c}{\partial t} - \nabla \cdot \left(D_{ab} \nabla c \right) + \vec{u} \cdot \nabla c = R \tag{7}$$

COMPUTATIONAL SETUP AND VALIDATION

Figure 3 presents the schematic of the computational domain, where two identical droplets are centrally located on electrodes

TABLE 1 | The physical properties of the droplet.

Property	Definition	Value	Unit
μ	Dynamic viscosity	1.01 × 10 ⁻³	N · s/m ²
ρ	Density	996.93	kg/m ³
y	Surface tension coefficient	0.0728	N/m
θ_0	Initial contact angle	90	deg
$ heta_{min}$	Minimum contact angle	Depends on the scheme	deg
θ_{max}	Maximum contact angle	Depends on the scheme	deg
R ₀	Initial radius of the two droplets	Depends on the scheme	mm
<i>C</i> ₀	Initial concentration of the dyed droplet	5	μM
D _{ab}	Diffusivity of dye	8 × 10 ⁻⁷	m²/s

TABLE 2 | The nondimensional geometrical parameters of the computational domain.

Property	Definition	Valu	
Ē	Nondimensional length of the computational domain	8	
Ŵ	Nondimensional width of the computational domain	8	
<i>Η</i>	Nondimensional height of the computational domain	3.6	
D	Nondimensional initial distance between the center of the two droplets	3	
EL	Nondimensional length of the electrode in the x-direction	1.5	

1 and 2, and electrodes 3 and 4, respectively. The red and blue droplets refer to droplet with and without dye, respectively. The droplets consist of water, with their physical properties listed in **Table 1**. The initial droplets are hemispheres with a radius of R_0 . The domain size is non-dimensionalized based on the initial droplet radius R_0 , which serves as the reference length scale; the corresponding geometrical parameters are detailed in **Table 2**.

Adaptive mesh refinement, known to optimize computational efficiency and accuracy for transient flows, is employed with a two-level approach. The simulation utilizes a uniform square mesh with a base grid spacing of $R_0/5$, determined by a grid refinement study. Near the droplet interface, the mesh is refined to 1/4 of the base grid spacing. Boundary conditions include a Navier slip at the domain bottom and no-slip conditions at the top and sides.

To ensure numerical stability across capillarity, viscosity, and Courant criteria, the time step is dynamically adjusted [33]. Mesh independence is confirmed by simulating with mesh sizes of $R_0/16$, $R_0/20$, and $R_0/25$ near the interface for 00.009 s for Case R1.12-60-90. Detailed mesh independence study can be found in our previous work [27]. Finally, a mesh size of $R_0 = 20$ near the interface is chosen and implemented in all the simulations.

RESULTS AND DISCUSSION

This study mainly focuses on the oscillation of the merged droplet. Hence, the simulated merging process is not presented. The onset of parametric instability within the droplet initiates lateral and vertical wave formation, leading to a star-shaped oscillatory pattern and surface undulations. This phenomenon has been investigated in several researches [34–39]. Research on initiating parametric **TABLE 3** | The cases used in the study. The name of the case refers to its initial radius of the two droplets R_0 , maximum contact angle θ_{max} , and minimum contact angle θ_{min} .

Name	R ₀ (mm)	$ heta_{max}$ (°)	$ heta_{min}$ (°)
Case R2-30-60	2	60	30
Case R1.34-30-60	1.34	60	30
Case R2-40-80	2	80	40
Case R2-60-90	2	90	60
Case R1.12-60-90	1.12	90	60

oscillations within micro-droplets in electrowetting-on-dielectric (EWOD) microfluidic systems has been documented in the literature [24, 40]. Bansal et al. have induced parametric oscillation in coalesced droplets, which markedly enhances the mixing efficiency and slashes the diffusive mixing time by as much as 98% [24]. The oscillatory behavior of the droplet's shape gives rise to distinct flow patterns, which merit further elaboration. The flow dynamics are examined numerically and compared with existing literature to ascertain the accuracy of the findings. Furthermore, the study presents and contrasts the vortices and shear rate distributions in the presence and absence of oscillations, thereby elucidating the flow dynamics induced by electrowetting-driven oscillations.

Multiple cases are studied to ensure the validity of our results. The cases studied here are listed in **Table 3** and referred to by their names in the following paragraphs for simplicity. The name of the case refers to its initial radius of the two droplets R_0 , maximum contact angle θ_{max} , and minimum contact angle θ_{min} .

To enhance clarity in the presentation of results, certain data have been rendered dimensionless. This normalization can be discerned by noting the presence of horizontal lines above the respective data headers, for example, \bar{x} represents the scaled



FIGURE 4 A cycle of the parametrically oscillating droplet at n = 5 mode, taking Case R1.34-30-60, n = 5 mode as an example. The phase of each droplet in a cycle is: (A) *T*, (B) *T*/4, (C) *T*/2, (D) 3*T*/4, (E) *T*, where *T* refers to a period of the droplet oscillation. (F) is the bottom view of the droplet, showing that the droplet radius R_b can be decomposed into R_a and η_{∞} .



horizontal coordinate. Unless otherwise specified, length-related parameters are scaled using R_0 , time parameters are scaled using the capillary timescale $t_c = \sqrt{\rho R_0^3 \gamma}$, and frequency-related parameters are scaled using $1/t_c$.

Parametric Oscillation

By subjecting the droplet to a driving frequency f_d that is twice its resonance frequency f_n under enough amplitude, parametric instability can be triggered in droplet. The



FIGURE 6 Streamline patterns at the base of the droplet for Case R2-60-90 in the n = 2 mode at a driving frequency of $f_d = 55$ Hz. The depicted phases of the droplet within its oscillation cycle are: (A) T/8, (B) T/4, and (C) 3T/8, with T denoting the oscillation period of the droplet.









oscillation mode number is marked as n. One characteristic of the parametric instability is the periodic lateral wave that appear in the azimuthal direction of the droplet. Figure 4F

is a bottom view of the droplet, where the droplet radius R_b can be regarded as a superposition of the equatorial radius R_a and the lateral disturbance η_{xx} .



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The theoretical resonance frequency of the sessile droplet can be estimated according to **Equations 8**, **9**:

$$\omega_n = \beta \sqrt{\frac{n(n-1)(n+2)\gamma}{\rho R_a^3}}$$
(8)

$$f_n = \frac{\omega_n}{2\pi} \tag{9}$$

Where ω_n is the angular resonance frequency, γ is the surface tension coefficient, ρ is the density of the droplet, R_a is the time-varying equatorial radius, n is the mode number, and β is the modification parameter, which ranges from 0.7 to 1 in our study. The mode number n also implicates the number of lobes that

appears in the star-shaped droplet. Up to eight modes of parametric oscillations are founded in this study.

The temporal evolution of the lateral wave is depicted in Figure 4, aligning closely with previously published findings [37, 38]. The oscillation period is identified as T. The moment at which the droplet achieves its most star-like form is designated as t_{star} and is considered the onset of the cycle, as illustrated in Figure 4A. Subsequently, the star-shaped droplet initiates the process of contracting its elongated lobes while elongating its shorter lobes. Over time, the droplet's base transforms into a spherical shape, with the lateral wave reaching zero amplitude, as shown in **Figure 4B** at T/4. The previous short and long lobes continue their respective processes of elongation and contraction, culminating in a star droplet that is the inverse of its initial state, as depicted in Figure 4C. For the sake of clarity, the initial star droplet configuration is referred to as star⁺, while the droplet's configuration at T/2 is designated as star⁻. Between T/2 and T, the droplet undergoes a symmetrical shape transformation, ultimately reverting to the star+ configuration, as shown in Figures 4D, E.

Calculation of the Most Star-Like Moment for Droplet

The instant at which the droplet reaches its most pronounced starshaped form is denoted as t_{star} , serving as a reference for identifying the full oscillation cycle of the star-shaped droplet. As the droplet undergoes continuous changes in its equatorial radius R_a , a modified measure of standard deviation, denoted $\bar{\sigma}(t)$, is proposed for the determination of t_{star} , as outlined in **Equation 10**. Here, the standard deviation $\sigma(t)$ is normalized by the equatorial radius $R_a(t)$. This normalization serves to remove the variability caused by the changing $R_a(t)$. The adjusted standard deviation $\bar{\sigma}(t)$ quantifies the deviation of the droplet from a spherical shape, with t_{star} corresponding to the peak value of $\bar{\sigma}(t)$. To calculate $\bar{\sigma}(t)$, data from the droplet's stable oscillatory state are utilized, with t_{star} is identified at the points of local maxima.







mode, $\bar{f}_d = 1.42$ (D) n = 7 mode, $\bar{f}_d = 1.77$.

$$\bar{\sigma}(t) = \frac{1}{R_a(t)} \sqrt{\frac{\sum_{i=1}^{N} \left(R_{b,i}(t) - R_a(t) \right)^2}{N}}$$
(10)

Flow Analysis

The parametric oscillation brings about not only shape changes, but also characteristic internal flow patterns, which will be discussed in the following paragraphs.

Validation

The internal flow in parametrically oscillating star-shaped droplet can be assumed as potential flow [41]. The radial internal flow velocity v_r in the bottom of the droplet can be expressed as follows:

$$v_r = -V_n \left(\frac{r}{R_a}\right)^{n-1} \cos\left(n\varphi\right) \sin\left(\omega_n t\right),\tag{11}$$

In **Equation 11**, V_n represents the peak fluid velocity observed at the equatorial periphery as the droplet returns to its equilibrium form. Additionally, r denotes the radial distance from the droplet's center, while φ specifies the azimuthal angle.

The distribution of the radial velocity v_r at the base of the droplet is illustrated in Figure 5A. Here, the droplet is in the T/4 phase, and the radial velocity exhibits a sinusoidal pattern around its circumference, characterized by the presence of eight wave crests. **Figure 5B** depicts the variation of the measured radial velocity v_r as a function of the azimuthal angle. The sinusoidal nature of the curve and the number of crests are in excellent agreement with the predictions of Equation 11, confirming that the flow dynamics observed in this study are consistent with the potential flow theory proposed in the literature [41] for parametric oscillations of droplets. The streamlines at the bottom of the droplet for Case R2-60-90, with a driving frequency of $f_d = 55$ Hz and at the n = 2 mode, are presented in Figure 6. This figure reveals a strong correlation with the experimental particle trace observations reported in the literature [41] for droplets undergoing parametric oscillations at the n = 2 mode.

Vortex and Shear Rate Analysis

The internal flow in the droplet includes flows in two directions, the up-down direction and the azimuthal direction, which can be



seen by the streamlines in the x-y plane and x-z plane, respectively. The streamlines radiating from the center in **Figure 7B** correspond to the droplet's flow at the bottom center reflected in **Figure 7A**. Therefore, this part of the streamlines in **Figure 7B** is not connected to the streamlines at the edge of the droplet, exhibiting a discontinuous pattern.

Cases excited with parametric oscillation show higher vorticity magnitude and shear rate than cases with no actuated oscillation and no parametric oscillation, as shown in **Figure 8**. Case R2-40-80 display n = 5 mode parametric oscillation at $f_d = 165$ Hz, and display no parametric oscillation mode at $f_d = 175$ Hz, whose driving frequency is close to $f_d = 165$ Hz. The former case shows stronger vorticity and shear rate than the later in the liquid-gas interface of the droplet [**Figures 8A, C, D, F**]. This may due to the higher oscillation amplitude brought about by the resonance mode, which also explains why Case R2-40-80 show higher vorticity and shear rate than cases with no actuated oscillation [**Figures 8A, B, D, E**].

Also, the distribution of the vortices and shear rate is worth studying. The vortices rarely appears inside the droplet, owing to the laminar nature of the micro-droplet. Nevertheless, there are still strong vortices near the liquid-gas interface of the droplet, most of which are distributed around the intersections of its lobes. This rule applies to all parametric oscillation cases studied here, as shown in **Figures 9A~F**. In the bottom plate, the temporal change of contact angle result in intense velocity gradient in the liquid air interface, [**Figure 5**] which may cause rotations of the fluid microelements and generate vortices around the liquid-gas interface. Considering t =

T/4 to T/2 when the previous short and long lobes continue their respective processes of elongation and contraction [**Figures 4B, C**], the velocity directions of two adjacent lobes are opposite to each other. Therefore, the velocity gradient at the intersection of two adjacent lobes is the greatest, which explains why the vorticity magnitude is mainly concentrated at these intersections. The shear rate are mainly located near and inside the liquid-gas interface [**Figures 10A~F**]. This can also be explained by the extension and retraction of the droplet brought about by the parametric oscillation. Due to the change in the curvature of the droplet, the interfacial tension generates an inward or outward pressure, resulting in stronger shear rate within the droplet.

The Mixing Process

In this section, the impact of the parametric oscillation on the mixing process is analyzed. We studied the dye distribution in droplets and defined the mixing index *MI* by scaling the variance σ_c^2 of the chemical concentrations in the transient regime [27, 42] as shown in **Equations 12**, 13:

$$\sigma_c^2 \coloneqq \frac{1}{N_{\text{tot}}} \oint_V \left(c\left(x, y, z, t\right) - \bar{c}\left(t\right) \right)^2 \mathrm{d}V, \tag{12}$$

$$MI \coloneqq 1 - \frac{\sigma_c^2}{\bar{c}},\tag{13}$$

Where $N_{\text{vol}}(t) \coloneqq \oint_V c(x, y, z, t) dV$ corresponds to the amounts of molecules in the volume, and \overline{c} is the mean



concentration. The mixing index MI ranging from 0 to 1 represents the mixing efficiency, and reaches 1 when the dye in the droplet is fully mixed.

Mixing Enhancement Achieved by Parametric Oscillation

At $\bar{t} = 45.71$, the droplet is almost mixed for Case R2-30-60 and Case R1.34-30-60, and the corresponding mixing index is marked as $MI_{45.71}$. Cases where droplet is not applied with AC voltage and oscillates freely are denoted as free oscillation. The mixing efficiency of the AC voltage-actuated oscillation cases and the free oscillation cases are compared by checking their mixing index MI at $\bar{t} = 45.71$, as shown in **Figure 11**. The cases with AC voltage-actuated oscillation, which is in good agreement with previous numerical and experimental studies [19, 21, 24, 27]. Hence, the parametric oscillation actuated by the AC voltage can be applied to enhance mixing in micro-droplet. It has been mentioned in *Vortex and Shear Rate Analysis* that the vorticity magnitude and

shear rate in parametric oscillation cases are higher than that in free oscillation cases. The vortices mainly distribute around the liquid-gas interface of the droplet, accelerating the mass transfer near the interface, and hence attribute to the overall increase of the mixing index. The shear rate distributed near and inside the liquid-gas interface can lead to the stretching and compression of fluid micro-elements, thereby disrupting the laminar structure within the fluid and promoting the mixing between different components. In summary, compared to free oscillation cases, parametric oscillation brings about higher vorticity magnitude and shear rate near the droplet liquid-gas interface, which enhances the mixing efficiency.

The Mixing Index Fluctuation

Besides the mixing enhancement, the parametric oscillation also introduces fluctuations in the mixing index MI curve, as shown in **Figure 12A**. The n = 2 parametric mode is excited at $\bar{f}_d = 0.58$ for Case R2-60-90, which are denoted as resonance in **Figure 12A**. The parametric mode case show fluctuation in

the MI curve, while the free oscillation and no resonance cases do not. This rule applies to all cases computed in this study. The original MI curve was processed to obtain a smoothed version using the locally weighted scatter plot smooth method implemented in MATLAB. This smoothing procedure allowed for the extraction of the fluctuation patterns from the original MIcurve, thereby providing a method to quantify the fluctuations introduced by the parametric oscillation. The fluctuations in MIcurve are referred to as MI_{osc} in the following text.

The mixing index MI curves for Case R1.34-30-60 and its corresponding free oscillation case are plotted in Figure 12B. Except the free oscillation case, all parametric oscillation cases show apparent mixing index fluctuations MI_{osc}. Applying FFT (Fast-Fourier Transformation) to the mixing index fluctuation MIosc, the main fluctuating frequency of MIosc show good agreement with its driving frequency f_d , as shown in Figure 13. This finding also validate that the mixing index fluctuation is introduced by the parametric oscillation. The mechanism of how parametric oscillation brings about this mixing index fluctuation MIosc is demonstrated by analyzing the dye distribution of the droplet. The dye distribution for Case R1.34-30-60, n = 5 mode is plotted in **Figure 14**, with positions of four dve lobes marked from 1 to 4 for further discussion. Dve lobes refer to the lobe shape that appear in the dye distribution, which is different from the lobes used when describing the shape of the star-shaped droplet. Between T/4 and T/2, the droplet undergoes a transformation from a spherical to a star⁺ configuration (Figures 14A-C). This morphological transition leads to the progressive convergence of dye lobes 2 and 3, which are increasingly compressed and eventually coalesce into a unified lobe, as depicted in Figure 14C. Subsequently, during the interval from 3T/4 to T, the droplet shifts from a spherical to a star⁻ shape (Figures 14D-F). In a similar manner, dye lobes 1 and 2 merge into one lobe, while dye lobes 3 and 4 amalgamate into a separate lobe, as illustrated in Figure 14F. According to these procedures, the mixing index may reach local maximum at T/2 or T since some dyes are compressed into one lobe, which explains the origin of the mixing index fluctuation MIosc. The intimate relationship between MIosc and the droplet's shape transformation suggests that the primary oscillation frequency of MI_{osc} should be twice that of the parametric oscillation frequency, f_{osc} , which is equivalent to the driving frequency, f_d . This frequency prediction aligns with the Fast Fourier Transform (FFT) results presented in Figure 13. The moment of the most star-like moment, t_{star}, should also corresponds to the local peak of the mixing index, or the crest of MI_{osc} . This is confirmed by Figure 15. Therefore, the proposed mechanism, whereby parametric oscillation induces MI_{osc} fluctuations by consolidating dye lobes into a unified shape, is consistent with the FFT characteristics and the correspondence of the MI_{osc} curve peaks to t_{star} .

CONCLUSION

This study utilizes numerical simulations to investigate how electrowetting-induced parametric oscillations enhance mixing

within a merged micro-droplet in Electrowetting-on-Dielectric (EWOD) microfluidic systems. It replicates a realistic scenario in EWOD digital microfluidics, where two micro-droplets collide head-on and merge, after which an AC voltage is applied to induce oscillations that improve mixing efficiency [15]. These parametric oscillations are intentionally triggered at specific frequencies and amplitudes. One of the droplets contains dye, allowing the mixing process to be meticulously examined through the distribution of dye concentration. The objective of this work is to numerically explore the mechanism by which parametric oscillation affects the mixing process of micro-droplets in EWOD devices, an area previously uninvestigated in the literature to the best of our knowledge. The following conclusions are drawn from the results presented:

First, the presence of parametric oscillation significantly influences the distribution and intensity of vortices and shear rate within the droplet flow field. The internal flow of the droplet exhibits directional characteristics in both the up-down and azimuthal directions. Parametric oscillation, particularly in resonance mode, enhances vorticity magnitude and shear rate at the liquid-gas interface compared to cases without actuated oscillation. Vortices are predominantly concentrated near the intersections of the droplet's lobes, with minimal appearance inside the droplet due to its laminar nature. The shear rate are primarily localized near and inside the liquid-gas interface, influenced by the droplet's extension and retraction caused by parametric oscillation.

Second, parametric oscillation is proven as an effective method for enhancing mixing in micro-droplets compared to free oscillation. At $\bar{t} = 45.71$, droplets under AC voltage-actuated oscillation, particularly in Cases R2-30-60 and R1.34-30-60, exhibit near-complete mixing, as indicated by the mixing index $MI_{45.71}$. This is in contrast to free oscillation cases where no AC voltage is applied. The heightened vorticity and shear rate near the liquid-gas interface, a result of parametric oscillation, are key factors contributing to the enhanced mixing. Vortices near the interface accelerate mass transfer, while shear rate disrupt the fluid's laminar structure, promoting intercomponent mixing.

Finally, it is highlighted that parametric oscillation not only enhances mixing but also introduces significant fluctuations in the mixing index (MI) curve. These fluctuations, termed MI_{osc} , are evident in all parametric oscillation cases studied, invisible for free oscillation and no parametric oscillation cases. The smoothed MI curves, obtained through the locally weighted scatter plot smooth method, reveal the fluctuation patterns induced by parametric oscillation. The main fluctuating frequency of MI_{osc} aligns with the driving frequency fd, confirming the role of parametric oscillation in generating these fluctuations. The mechanism behind *MIosc* is explained through the analysis of dye distribution within the droplet, showing how the droplet's shape transformation from spherical to star-shaped configurations leads to the convergence and coalescence of dye lobes, resulting in local maxima of the mixing index. The frequency of MIosc is predicted to be twice that of the parametric oscillation frequency, which is consistent with FFT results and the correlation between the peaks of MIosc and the

most star-like moment (t_{star}) . This proposed mechanism provides a comprehensive understanding of how parametric oscillation influences the mixing process in droplets.

Ultimately, this research underscores the potential of parametric oscillation as a powerful tool for enhancing mixing in micro-droplets within EWOD systems. The detailed insights into the mechanisms behind mixing index fluctuations provide a novel understanding of droplet mixing dynamics, which can be directly applied to improve the design and operation of microfluidic devices for applications requiring efficient and controlled mixing processes.

DATA AVAILABILITY STATEMENT

The original contributions presented in the study are included in the article/supplementary material, further inquiries can be directed to the corresponding author.

AUTHOR CONTRIBUTIONS

The first author, YW, conceptualization, methodology, numerical computation, and draft writing. The second author, JZ, funding acquisition, project administration, supervision, and draft reviewer. The third author, ZZ, investigation and

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CONFLICT OF INTEREST

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GENERATIVE AI STATEMENT

The author(s) declare that no Generative AI was used in the creation of this manuscript.

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